



Weakly Nonlinear Convection of a Maxwell Fluid in a Porous Layer With Coriolis Effect

C. Bheemudu¹ , T. Ramakrishna Goud¹ , M. Pavan Kumar Reddy*²  and P. Raghavendra³ 

¹Department of Mathematics, Osmania University, Telangana 500007, India

²Department of Humanities and Sciences, VNR Vignana Jyothi Institute of Engineering and Technology, Hyderabad 500090, India

³Department of Mathematics, Malla Reddy University, Hyderabad 500100, India

*Corresponding author: mprnitw@gmail.com

Received: September 28, 2022

Accepted: March 23, 2023

Abstract. The linear and non-linear instability theories of a Maxwell fluid in a Darcy-Benard setup with coriolis effect is studied. For linear theory, the method of normal modes has been employed to solve governing dimensionless equations which led an eigenvalue problem and it is solved analytically. We obtained the expressions for steady and oscillatory thermal Rayleigh numbers. The effects of different physical parameters on steady and oscillatory convective phenomena are presented and described. In order to study the heat transport by convection the well-known equation, Landau-Ginzburg equation has been derived.

Keywords. Porous media, Rotation, Maxwell fluid, Non-linear stability analysis

Mathematics Subject Classification (2020). 35Q56, 76E30, 76S05

Copyright © 2023 C. Bheemudu, T. Ramakrishna Goud, M. Pavan Kumar Reddy and P. Raghavendra. *This is an open access article distributed under the Creative Commons Attribution License, which permits unrestricted use, distribution, and reproduction in any medium, provided the original work is properly cited.*

1. Introduction

Double-diffusive convection is of important study due its practical applications in many geological processes. Also, this study has wide range of geotechnical applications, in particular, liquid re-injection, the migration, underground disposal of nuclear wastes, and drying processes (Chandrasekhar [5], Beckermann and Viskanta [4], Coriell *et al.* [6], Prescott and Incropera

[14], Zhou and Zebib [20], and Babu *et al.* [2, 3]). Similarly, Double-diffusive instability of a Newtonian fluid in a porous layer is well studied [13]. Similarly, convective phenomena in a porous layer saturated with non-Newtonian fluids is of interest due to its vast applications in science and engineering. Non-Newtonian fluids are frequently treated using the viscoelastic fluid model, power-law model, Maxwell fluid model etc. (see Dharmadhikari and Kale [7], Reddy and Ragoju [16], and Shenoy [17]).

Double-diffusive convection in a porous layer saturated by Oldroyd fluid was discussed by Malashetty and Swamy [11]. They obtained the analytical conditions for steady, overstable, and finite amplitude convective phenomena. Malashetty *et al.* [12] and Kumar and Bhadauria [10] extended the work done by Malashetty and Swamy [11] by considering thermal non-equilibrium effect. The double-diffusive convective motion of a Maxwell liquid was considered by Awad *et al.* [1]. They deduce that the minimal value of thermal Rayleigh number decreases with the Maxwell parameter. Wang and Tan [18] derived the condition for onset of convective instability of a non-Newtonian type liquid in a porous layer. They used modified Maxwell-Darcy model. Internally heated double-diffusive instability in a non-Newtonian type of coupled stress fluid in a porous layer was discussed by Gaikwad and Kouser [9].

Gaikwad and Dhanraj [8] discussed the effects of anisotropic and internal heating on the binary Maxwell liquid in a permeable layer. Reddy and Ragoju [15] studied the thermo solutal convection of a Maxwell fluid in a porous layer with the chemical reaction effect. They found that the Damkohler number has a contrast effect on steady and oscillatory convection. Yadav *et al.* [19] extended the work done by Reddy and Ragoju [15] by considering internal heat source.

In the present analysis, we consider linear and weakly non-linear instability theories of Maxwell fluid in a porous layer with coriolis effect. The organization of the present analysis is as follows: In Section 2, we describe the mathematical formulation. The linear stability analysis is described in Section 3. In Section 4, two dimensional amplitude equation is derived. The discussions of obtained results are presented in Section 5. In the last section, conclusions are written.

2. Mathematical Formulation

Let us assume a porous layer of maxwell fluid heated and salted from below, and zone placed between two infinitely, parallel, horizontal plates at $z = 0$ and $z = d$. The z -axis is oriented upward. It is rotating at a constant rate Ω . The governing equations under the Oberbeck–Boussinesq approximation are

$$\nabla \cdot \mathbf{u} = 0, \quad (1)$$

$$\left(1 + \lambda_1 \frac{\partial}{\partial t}\right) \left(\frac{\rho_0}{\phi} \frac{\partial \mathbf{u}}{\partial t} + \nabla P - \rho \mathbf{g}\right) + \frac{\mu}{\kappa} \mathbf{u} + \frac{2\rho_0 \Omega}{\phi} \widehat{e}_z \times \mathbf{u} = 0, \quad (2)$$

$$(\rho c)_m \frac{\partial \theta}{\partial t} + (\rho c)_f (\mathbf{u} \cdot \nabla) \theta = (\rho c)_m k T \nabla^2 \theta, \quad (3)$$

$$\rho = \rho_0 (1 - \alpha(\theta - \theta_0)), \quad (4)$$

$$\mathbf{u} = \theta = 0 \text{ on } z = 0, 1. \tag{5}$$

The conductive state of the Maxwell fluid is as follows:

$$\mathbf{u}_b = 0, \quad \rho = \rho_b(z), \quad \theta_b = \theta_0 - \left(\frac{\Delta\theta}{d}\right). \tag{6}$$

We introduce the dimensionless parameters as follows

$$\begin{aligned} (x, y, z) &= (x^* d, y^* d, z^* d), \\ (u, v, w) &= \left(\frac{\phi k}{d} u^*, \frac{\phi k}{d} v^*, \frac{\phi k}{d} w^*\right), \\ t &= \frac{d^2}{k} t^*, \quad p = \frac{\mu \phi k}{\kappa} p^*, \quad \theta = \Delta\theta \theta^*. \end{aligned} \tag{7}$$

Then the governing equations for non-dimensional quantities can be written as

$$\nabla \cdot \mathbf{u} = 0, \tag{8}$$

$$\left(1 + \lambda \frac{\partial}{\partial t}\right) \left(\frac{1}{Pr} \frac{\partial \mathbf{u}}{\partial t} + \nabla P - R \widehat{e}_z\right) + \mathbf{u} + Ta \widehat{e}_z \times \mathbf{u} = 0, \tag{9}$$

$$\frac{\partial \theta}{\partial t} + \gamma(\mathbf{u} \cdot \nabla)\theta = w + \nabla^2 \theta, \tag{10}$$

$$\mathbf{u} = \theta = 0 \text{ on } z = 0, 1, \tag{11}$$

where

$$\begin{aligned} R &= \frac{\rho_0 \delta \theta g \kappa d}{\mu \phi k_T}, \quad Ta = \left(\frac{2 \rho_0 \Omega d^2}{\mu}\right)^2 \\ Pr &= \frac{\mu \phi}{\rho_0 k_T}, \quad \lambda = \frac{\lambda_1 k_T}{d^2}, \\ \gamma &= \frac{(\rho c)_f}{(\rho c)_m} \phi. \end{aligned}$$

All quantities which are used in the above equations have been described in the nomenclature.

We now eliminate the pressure by taking the third component of curl of (9) and curl of curl of (9), one obtains

$$\left(1 + \lambda \frac{\partial}{\partial t}\right) \left(\frac{1}{Pr} \frac{\partial}{\partial t}\right) \omega_z + \omega_z - Ta \frac{\partial w}{\partial z} = 0, \tag{12}$$

$$\left(1 + \lambda \frac{\partial}{\partial t}\right) \left(\frac{1}{Pr} \frac{\partial}{\partial t}\right) (-\nabla^2 w) - \nabla^2 w + R \theta \left(1 + \lambda \frac{\partial}{\partial t}\right) (\nabla_h)^2 - Ta \frac{\partial \omega_z}{\partial z} = 0, \tag{13}$$

where $\omega_z = (\nabla \times \mathbf{V}) \cdot \widehat{e}_z$ and $\nabla_h^2 = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2}$.

By removing ω_z and θ from eqs. (12), (13), (10) one obtains,

$$\mathcal{L}w = \mathcal{N}, \tag{14}$$

where

$$\begin{aligned} \mathcal{L} &= \left(1 + \left(1 + \lambda \frac{\partial}{\partial t}\right) \left(\frac{1}{Pr} \frac{\partial}{\partial t}\right)\right) \left(\left(\frac{\partial}{\partial t} - \nabla^2\right) \nabla^2 + Ta \left(\frac{\partial}{\partial t} - \nabla^2\right) \frac{\partial^2}{\partial z^2}\right) \\ &+ \left(1 + \lambda \frac{\partial}{\partial t}\right) \left(\frac{1}{Pr} \frac{\partial}{\partial t} \left(\frac{\partial}{\partial t} - \nabla^2\right) \nabla^2 - R(\nabla_h)^2\right), \end{aligned} \tag{15}$$

$$\mathcal{N} = -R(\nabla_h)^2 \left(1 + \lambda \frac{\partial}{\partial t}\right) \left(1 + \left(1 + \lambda \frac{\partial}{\partial t}\right) \left(\frac{1}{Pr} \frac{\partial}{\partial t}\right)\right) \gamma(\mathbf{u} \cdot \nabla)\theta. \tag{16}$$

3. Linear Stability Analysis

Let us substitute $w = \sin \pi z e^{i(lx+my)+i\omega t}$ in $\mathcal{L}w = 0$, hence one obtains

$$R = \frac{(-i\delta^2 + \omega)(\pi^2 Pr^2 Ta^2 + \delta^2(Pr + \omega(i - \lambda\omega))^2)}{Pr q^2(-i + \lambda\omega)(Pr + \omega(i - \lambda\omega))}. \tag{17}$$

3.1 Stationary Convection

First, we consider stationary instability, i.e., $\sigma = 0$ is real. The stationary Rayleigh number R_s can be written as

$$R_s = \frac{\pi^2 Ta^2 \delta^2 + \delta^4}{q^2}. \tag{18}$$

3.2 Oscillatory Convection

Now consider the real and imaginary parts of R , which require the imaginary part of R to vanish. Substituting ω^2 into the real part of R yields the thermal Rayleigh number, R_T^{oc} , for oscillatory convection.

4. Weakly Non-linear Analysis

Let us introduce the following series expansion in terms of ϵ

$$\left. \begin{aligned} u &= \epsilon u_0 + \epsilon^2 u_1 + \epsilon^3 u_2 + \dots, \\ v &= \epsilon v_0 + \epsilon^2 v_1 + \epsilon^3 v_2 + \dots, \\ w &= \epsilon w_0 + \epsilon^2 w_1 + \epsilon^3 w_2 + \dots, \\ \theta &= \epsilon \theta_0 + \epsilon^2 \theta_1 + \epsilon^3 \theta_2 + \dots, \\ C &= \epsilon C_0 + \epsilon^2 C_1 + \epsilon^3 C_2 + \dots, \end{aligned} \right\} \tag{19}$$

where

$$\epsilon^2 = \frac{R - R_{sc}}{R_{sc}} \ll 1.$$

The first approximations are

$$\left. \begin{aligned} u_0 &= \frac{i\pi}{l_{sc}} [A e^{i(l_{sc}x + m_{sc}y)} \cos \pi z - c.c], \\ v_0 &= \frac{\pi}{il_{sc}} [A e^{i(l_{sc}x + m_{sc}y)} \cos \pi z - c.c], \\ w_0 &= [A e^{i(l_{sc}x + m_{sc}y)} \sin \pi z + c.c], \\ \theta_0 &= \frac{\gamma}{\delta_{sc}^2} [A e^{i(l_{sc}x + m_{sc}y)} \sin \pi z + c.c], \end{aligned} \right\} \tag{20}$$

where the amplitude, $A = A(X, Y, Z, T)$, is the amplitude and the complex conjugate is denoted by $c.c$. The variables X, Y, Z and T can be scaled as

$$X = \epsilon x, \quad Y = \epsilon^{\frac{1}{2}} y, \quad Z = z, \quad T = \epsilon^2 t,$$

Using the above scaling differential operators can be written as

$$\left. \begin{aligned} \frac{\partial}{\partial x} &\rightarrow \frac{\partial}{\partial x} + \epsilon \frac{\partial}{\partial X}, \\ \frac{\partial}{\partial y} &\rightarrow \frac{\partial}{\partial y} + \epsilon^{\frac{1}{2}} \frac{\partial}{\partial Y}, \\ \frac{\partial}{\partial z} &\rightarrow \frac{\partial}{\partial Z}, \\ \frac{\partial}{\partial t} &\rightarrow \epsilon^2 \frac{\partial}{\partial T}. \end{aligned} \right\} \tag{21}$$

By using eq. (21), the operators \mathcal{L} and \mathcal{N} of eq. (14) can be written as

$$\left. \begin{aligned} \mathcal{L} &= \mathcal{L}_0 + \epsilon \mathcal{L}_1 + \epsilon^2 \mathcal{L}_2 \dots, \\ \mathcal{N} &= \mathcal{N}_0 + \epsilon \mathcal{N}_1 + \epsilon^2 \mathcal{N}_2 \dots. \end{aligned} \right\} \tag{22}$$

On substituting eq. (22) into eq. (14), and comparing the coefficients of ϵ , ϵ^2 and ϵ^3 , one obtains

$$\mathcal{L}_0 w_0 = 0, \tag{23}$$

$$\mathcal{L}_0 w_1 + \mathcal{L}_1 w_0 = \mathcal{N}_0, \tag{24}$$

$$\mathcal{L}_0 w_2 + \mathcal{L}_1 w_1 + \mathcal{L}_2 w_0 = \mathcal{N}_1. \tag{25}$$

where

$$\mathcal{L}_0 = -\nabla^4 - R \nabla_h^2 - D^2 \nabla^2 T\alpha, \tag{26}$$

$$\mathcal{L}_1 = 2 \frac{\partial^2}{\partial x \partial X} (-2\nabla^2 - R - D^2 T\alpha), \tag{27}$$

$$\begin{aligned} \mathcal{L}_2 &= \frac{\partial^2}{\partial X^2} (-2\nabla^2 - R - D^2 T\alpha) + \left(2 \frac{\partial^2}{\partial x \partial X}\right)^2 (\nabla^2 - D^2 T\alpha) \\ &\quad + \frac{\partial}{\partial \tau} \left(\nabla^2 + D^2 T\alpha - R \lambda \nabla_h^2 - \frac{1}{Pr} (2\nabla^4 - R \nabla_h^2)\right). \end{aligned} \tag{28}$$

Let us substitute the solution w_0 in to $\mathcal{L}_0 w_0 = 0$. One obtains

$$R_{sc} = \frac{\pi^2 T\alpha^2 \delta^2 + \delta^4}{q^2}, \tag{29}$$

from the equation $\mathcal{L}_0 w_1 + \mathcal{L}_1 w_0 = \mathcal{N}_0$, $\mathcal{N}_1 = 0$ and $\mathcal{L} w_0 = 0$. The equation reduces to $w_1 = 0$, which implies $u_1 = 0$, and also,

$$\theta_1 = \frac{\gamma}{2\pi \delta_{sc}^2 \pi} |A|^2 \sin 2\pi z. \tag{30}$$

On substituting the first order solutions into the eq. (25), we obtain Newell-Whitehead equation in the form of

$$\lambda_0 \frac{\partial A}{\partial T} - \lambda_1 \left(\frac{\partial}{\partial X} - \frac{i}{2q_{sc}} \frac{\partial^2}{\partial Y^2}\right)^2 A - \lambda_2 A + \lambda_3 |A|^2 A = 0, \tag{31}$$

where

$$\lambda_0 = R_{sc} \lambda q_{sc}^2 - \delta_{sc}^2 - \pi^2 T\alpha - \frac{1}{Pr} (2\delta_{sc}^4 + R_{sc} q_{sc}^2),$$

$$\lambda_1 = 2\delta_{sc}^2 - R_{sc} + \pi^2 T\alpha,$$

$$\begin{aligned} \lambda_2 &= -\delta_{sc}^4 + R_{sc}q_{sc}^2 - \pi^2 Ta \delta_{sc}^2, \\ \lambda_3 &= \frac{\gamma}{2\pi\delta_{sc}^2} R_{sc}q_{sc}^2. \end{aligned} \tag{32}$$

Dropping t and y -dependence terms in the eq. (31), one obtains

$$\frac{d^2A}{dX^2} + \frac{\lambda_2}{\lambda_1} \left(1 - \frac{\lambda_3}{\lambda_1} |A|^2\right) A = 0. \tag{33}$$

Therefore,

$$A(x) = A_0 \tanh\left(\frac{x}{\Lambda_0}\right), \tag{34}$$

where

$$A_0 = \left(\frac{\lambda_2}{\lambda_3}\right)^{\frac{1}{2}} \quad \text{and} \quad \Lambda_0 = \left(\frac{2\lambda_1}{\lambda_2}\right)^{\frac{1}{2}}.$$

4.1 Heat Transport by Convection

From equation (34), we obtain maximum of steady amplitude A ($|A_{\max}|$) as

$$|A_{\max}| = \left(\frac{\epsilon^2 \lambda_2}{\lambda_3}\right)^{\frac{1}{2}}. \tag{35}$$

We define the Nusselt number in terms of amplitude A as

$$Nu = 1 + \frac{\epsilon^2}{\delta_{sc}^2} |A_{\max}|^2. \tag{36}$$

From eq. (36), we obtain convection for $R > R_{sc}$ and conduction for $R \leq R_{sc}$. Eq. (31) is valid for $\lambda_3 > 0$ which is possible when $R > R_{sc}$, Thus we get

- (i) convection for $Nu > 1$,
- (ii) conduction for $Nu \leq 1$ (see in Figure 1).

5. Results and Discussions

In the present analysis, the numerical results and conclusions are presented. The linear and non-linear instability of Darcy-Benard setup saturated by a Maxwell fluid with rotation confined between two horizontal boundaries is studied. The linear instability threshold parameters consisting of the Rayleigh number R , Taylor number Ta , relaxation parameter λ and Prandtl number Pr are shown in Table 1-3.

Table 1. Critical Rayleigh number at the onset of stationary convection versus Taylor number

Ta	R_c^{sc}	Ta	R_c^{sc}	Ta	R_c^{sc}
400	1618520.3233	2400	58252032.2439	4400	195790561.1939
800	6472821.3451	2800	79287336.6715	4800	233006869.0274
1200	14563323.0480	3200	103558841.7804	5200	273459377.5421
1600	25890025.4321	3600	131066547.5704	5600	317148086.7380
2000	40452928.4974	4000	161810454.0415	6000	364072996.6150

Table 2. Critical Rayleigh number at the onset of oscillatory convection versus Ta fixed at $\lambda = 0.8$

	$Pe = 0.001$	$Pe = 0.01$	$Pe = 0.1$
Ta	R_c^{oc}	R_c^{oc}	R_c^{oc}
400	20213002.8335	1999590.0068	178835.4255
800	20212015.9025	1999403.4566	178917.9303
1200	20211054.0222	1999348.9338	179055.9854
1600	20210206.9685	1999337.3702	179248.6488
2000	20209476.0403	1999345.0151	179495.1632
2400	20208846.7657	1999363.9661	179794.6591
2800	20208303.9211	1999391.0889	180146.0610
3200	20207834.2074	1999424.9620	180548.1727
3600	20207426.4861	1999464.8709	180999.6829
4000	20207071.5092	1999510.4265	181499.0948

Table 3. Critical Rayleigh number at the onset of oscillatory convection versus λ fixed at $Ta = 800$

	$Pe = 0.001$	$Pe = 0.01$	$Pe = 0.1$
λ	R_c^{oc}	R_c^{oc}	R_c^{oc}
0.50	1190331.2286	116794.0248	13552.3204
0.55	2122849.7122	209444.1885	21095.4959
0.60	3588517.0008	354891.1087	33642.2843
0.65	5808631.4859	574942.4725	53115.7906
0.70	9066983.7370	897556.2319	81793.8314
0.75	13720716.0801	1357884.8303	122543.6830
0.80	20212015.9025	1999403.4566	178917.9303
0.85	29080674.0240	2875120.1685	255218.1061
0.90	40977506.7848	4048867.3903	356563.3972
0.95	56678623.8238	5596675.0544	488966.2117

The behavior of critical Rayleigh number at the onset of stationary convection R_c^{sc} versus Ta is displayed in Table 1. In this table, enhancing of R_c^{sc} with the enhancement in the value of Ta is observed. Hence R_c^{sc} has a stabilizing effect on the system.

Table 2 shows that change of critical Rayleigh number at the onset of oscillatory convection R_c^{oc} with Ta for different values of Pe and for fixed value of $\lambda = 0.8$. This table shows that, Ta increases as R_c^{oc} decreases at $Pe = 0.001$. Also, at $Pe = 0.01$, increasing of Ta the value of R_c^{oc} is monotonically decreasing as well as increasing at certain point, but it is different at $Pe = 0.1$, that is Ta increases as R_c^{oc} increases.

Table 3 depicts the variation of R_c^{oc} versus λ for different values of Pe with other parameters held constant. In this table, the enhancement of R_c^{oc} is observed with the increase in the value of λ and Pe . As a result, λ and Pe have a stabilizing effect on the system.

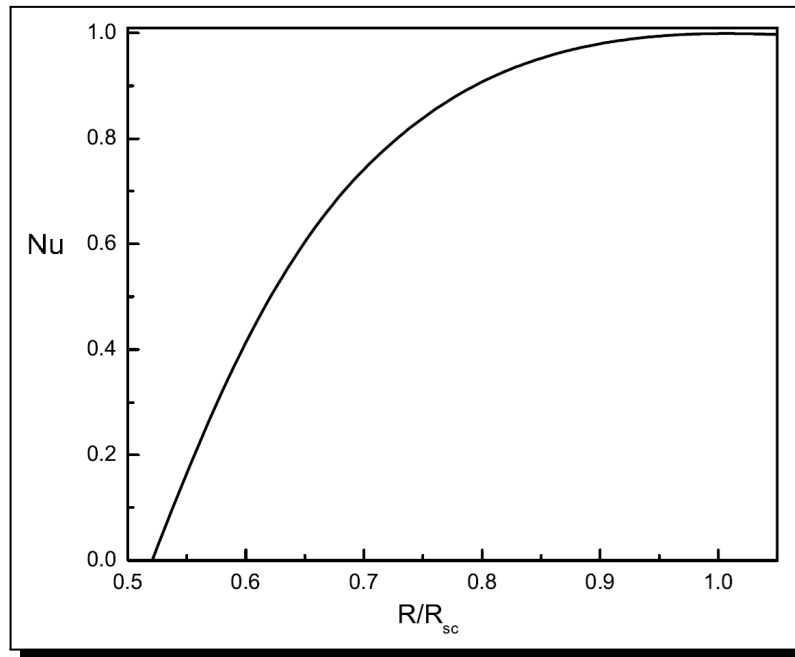


Figure 1. The figure is plotted for the fixed values of $Ta = 50$, $\lambda = 0.5$, $Pr = 5$

6. Conclusion

In this study, we have examined the linear and non-linear instability of Darcy-Benard setup saturated by a Maxwell fluid with rotation. The behaviour of various parameters like the Rayleigh number R , Taylor number Ta , relaxation parameter λ , wavenumber q , relaxation parameter γ and Prandtl number Pr have been analysed. The results can be summarized as follows:

- For oscillatory convection, the critical Rayleigh number increases with as increase in relaxation parameter by varying different Prandtl number, which is stabilizing factor to make the system more stable.
- For stationary convection, the critical thermal Rayleigh number increases with as increase in the Taylor number, which is stabilizing factor to make the system more stable.

Nomenclature

\bar{V}	Fluid velocity	k_T	Thermal diffusivity
u, v, w	velocity components	κ	Permeability
Ω	Angular Velocity	d	Length
θ	Temperature	<i>Dimensionless Parameters</i>	
t	Time	A	Complex Amplitude
P	Pressure	R	Rayleigh number
g	acceleration due gravity		

Ta	Hartmann number	<i>Greek Symbols</i>	
λ	relaxation parameter	α	Thermal expansion coefficient
Pr	Prandtl number	ϵ	Porosity
q	Wave number	ρ	Fluid density
Nu	Nusselt number	ν	Kinematic viscosity

Competing Interests

The authors declare that they have no competing interests.

Authors' Contributions

All the authors contributed significantly in writing this article. The authors read and approved the final manuscript.

References

- [1] F. G. Awad, P. Sibanda and S. S. Motsa, On the linear stability analysis of a Maxwell fluid with double-diffusive convection, *Applied Mathematical Modelling* **34**(11) (2010), 3509 – 3517, DOI: 10.1016/j.apm.2010.02.038.
- [2] A. B. Babu, G. S. K. Reddy and S. G. Tagare, Nonlinear magneto convection due to horizontal magnetic field and vertical axis of rotation due to thermal and compositional buoyancy, *Results in Physics* **12** (2019), 2078 – 2090, DOI: 10.1016/j.rinp.2019.02.022.
- [3] A. B. Babu, G. S. K. Reddy and S. G. Tagare, Nonlinear magnetoconvection in a rotating fluid due to thermal and compositional buoyancy with anisotropic diffusivities, *Heat Transfer* **49**(1) (2020), 335 – 355, DOI: 10.1002/htj.21615.
- [4] C. Beckermann and R. Viskanta, Double-diffusive convection during dendritic solidification of a binary mixture, *Physicochemical Hydrodynamics* **10**(2) (1988), 195 – 213.
- [5] S. Chandrasekhar, *Hydrodynamic and Hydrodynamic Stability*, Clarendon Press, Oxford University, 652 pages (1961).
- [6] S. R. Coriell, M. R. Cordes, W. J. Boettinger and R. F. Sekerka, Convective and interfacial instabilities during unidirectional solidification of a binary alloy, *Journal of Crystal Growth* **49**(1) (1980), 13 – 28, DOI: 10.1016/0022-0248(80)90056-1.
- [7] R. V. Dharmadhikari and D. D. Kale, Flow of non-Newtonian fluids through porous media, *Chemical Engineering Science* **40**(3) (1985), 527 – 528, DOI: 10.1016/0009-2509(85)85113-7.
- [8] S. Gaikwad and M. Dhanraj, Onset of double diffusive convection in a maxwell fluid saturated anisotropic porous layer with internal heat source, *Special Topics & Reviews in Porous Media: An International Journal* **4**(4) (2013), 359 – 374, DOI: 10.1615/SpecialTopicsRevPorousMedia.v4.i4.70.
- [9] S. N. Gaikwad and S. Kouser, Double diffusive convection in a couple stress fluid saturated porous layer with internal heat source, *International Journal of Heat and Mass Transfer* **78** (2014), 1254 – 1264, DOI: 10.1016/j.ijheatmasstransfer.2014.07.021.
- [10] A. Kumar and B. Bhadauria, Double diffusive convection in a porous layer saturated with viscoelastic fluid using a thermal non-equilibrium model, *Physics of Fluids* **23** (2011), 054101, DOI: 10.1063/1.3588836.

- [11] M. S. Malashetty and M. Swamy, The onset of double diffusive convection in a viscoelastic fluid layer, *Journal of Non-Newtonian Fluid Mechanics* **165**(19-20) (2010), 1129 – 1138, DOI: 10.1016/j.jnnfm.2010.05.011.
- [12] M. S. Malashetty, A. A. Hill and M. Swamy, Double diffusive convection in a viscoelastic fluid-saturated porous layer using a thermal non-equilibrium model, *Acta Mechanica* **223** (2012), 967 – 983, DOI: 10.1007/s00707-012-0616-1.
- [13] D. A. Nield and A. Bejan, *Convection in Porous Media*, 4th edition, Springer, New York, xxvi + 778 pages (2013), DOI: 10.1007/978-1-4614-5541-7.
- [14] P. Prescott and F. Incropera, Magnetically damped convection during solidification of a binary metal alloy, *ASME Journal of Heat and Mass Transfer* **115**(2) (1993), 302 – 310, DOI: 10.1115/1.2910680.
- [15] G. S. K. Reddy and R. Ragoju, Thermal instability of a maxwell fluid saturated porous layer with chemical reaction, *Special Topics & Reviews in Porous Media: An International Journal* **13**(1) (2022), 33 – 47, DOI: 10.1615/SpecialTopicsRevPorousMedia.2021037410.
- [16] G. S. K. Reddy and R. Ragoju, Thermal instability of a power-law fluid-saturated porous layer with an internal heat source and vertical throughflow, *Heat Transfer* **51**(2) (2022), 2181 – 2200, DOI: 10.1002/htj.22395.
- [17] A. V. Shenoy, Non-Newtonian fluid heat transfer in porous media, *Advances in Heat Transfer* **24** (1994), 101 – 190, DOI: 10.1016/S0065-2717(08)70233-8.
- [18] S. Wang and W. Tan, Stability analysis of solet-driven double-diffusive convection of Maxwell fluid in a porous medium, *International Journal of Heat and Fluid Flow* **32**(1) (2011), 88 – 94, DOI: 10.1016/j.ijheatfluidflow.2010.10.005.
- [19] D. Yadav, M. Al-Siyabi, M.K. Awasthi, S. Al-Nadhairi, A. Al-Rahbi, M. Al-Subhi, R. Ragoju and K. Bhattacharyya, Chemical reaction and internal heating effects on the double diffusive convection in porous membrane enclosures soaked with maxwell fluid, *Membranes* **12**(3) (2022), 338, DOI: 10.3390/membranes12030338.
- [20] H. Zhou and A. Zebib, Oscillatory double diffusive convection in crystal growth, *Journal of Crystal Growth* **135**(3-4) (1994), 587 – 593, DOI: 10.1016/0022-0248(94)90151-1.

